An Explicit Finite Difference Method

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Abstract—This paper presents a one dimensional advection diffusion equation (ADE) as a simple mathematical model for the estimation of river water pollution. The numerical solution of ADE is obtained by using explicit centered difference scheme with FTBSCS techniques for prescribed initial and boundary data which may be used to predict the contaminant concentration levels in a river. Numerical results for the scheme are compared in terms of accuracy by error estimation with an exact solution of the ADE, and also the numerical features of the rate of convergence are presented graphically. Computational result verifies the qualitative behavior of the solution of ADE for various considerations of the parameters.

Keywords—Advection Diffusion Equation, Finite Difference Scheme, Exact Solution, Stability Condition, Water pollution, Rate of Convergence.

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1. INTRODUCTION

iver water pollution can be modeled using one dimensional advection-diffusion equation (ADE). This equation reflects physical phenomena where in the diffusion process particles are moving with certain velocity from higher concentration to lower concentration. It is a partial differential equation of parabolic type, derived on the principle of conservation of mass using Fick's 1st law. Due to the growing surface and subsurface hydro-environment degradation and the air pollution, the advection-diffusion equation has drawn significant attention of hydrologists, civil engineers and mathematical modelers. The analytical/numerical solutions along with an initial condition and two boundary conditions help to understand the contaminant or pollutant concentration distribution behavior through an open medium like air, rivers, lakes and porous medium like aquifer. It has wide applications in other disciplines too, like soil physics, petroleum engineering, chemical engineering and biosciences.

Many researchers have already been worked on it. Ogata and Banks [7] obtained an analytical solution of the one dimensional ADE by reducing the original ADE into a diffusion equation by applying moving coordinates. Banks and Ali[12] obtained an analytical solution of the one dimensional ADE by reducing the original ADE into a diffusion equation by introducing another dependent variable. Atul Kumar, Dilip Kumar Jaiswal and Naveen Kumar [6] presented an analytical solution of the one dimensional ADE by reducing the original ADE into a diffusion equation by using Laplace transformation technique. Agusta and Bamingbola [8] studied on the numerical treatment of the mathematical model for water pollution. This study was examined by various mathematical models invoving water pollution. The authors used the implicit centered difference scheme in space and a forward difference scheme in ti

mefor the evaluation of the generalized transport equation.ChangiunZhu, LipingWa and Sha Li [20] presented a numerical simulation of hybrid finite analytic methods for ground water pollution. Changiun and Shuwen [21] made a numerical simulation on river water pollution by using grey differential model. They corrected the model in finding the truncation error and found that the obtained results from the grey model are excellent and reasonable. Thongmoon and Mckibbin [14] compared some numerical methods for the advection-diffusion equation. They reported that the finite difference methods (FTCS, Crank Nicolson) give better point-wise solutions than the spline methods. M. M. Rahman, L.S. Andallah [22] presented a simulation of water pollution by finite difference method. They estimated and analyzed the extent of water pollution at different time and points.

In the present paper our intention is to investigate mathematical models and subsequent numerical methods to predict the contaminant concentration levels in a river at different time and different points of water bodies.

2. GOVERNING equation

The one-dimensional advection-diffusion equation (1) is considered as water pollution model is given as

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2} \dots \dots \dots \dots (1)$$

where *c* represents the solute concentration [*ML*⁻³] at the point *x*, along longitudinal direction at time *t*, *D* is the solute dispersion, if it is independent of position and time, is called dispersion coefficient [L^2T^{-1}], *t* = time [*T*]; *x* = distance [*L*] and, *u* is the mean flow velocity [LT⁻¹] assumed to be constant.

Appended with initial condition

$$c(x,0) = f(x)0 \le x < l$$

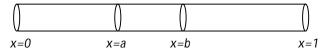
and boundary conditions

$$c(x = 0, t) = g_0(x)$$
 $0 < t \le T$
 $c(x = l, t) = g_l(x)$ $0 < t \le T$

the ADE formulates an initial boundary value problem (IBVP).

2.1 ADVECTION DIFFUSION EQUATION AND ITS DERIVATION

For our model we assumed that the advection-diffusion equation may be a good first approximation to model the river pollution levels. It was also assumed that the river had a uniform cross-sectional area. Therefore, the river was assumed to be linear or one-dimensional (a pipe with a uniform cross-sectional area).



A one-dimensional river cross-section with arbitrary interior and end points at x=0 and x=1.

The advection-diffusion equation in one dimension is

given by

$$c_t = Dc_{xx} - uc_x + f \dots \dots \dots \dots (2)$$

where, the parameters are defined as follows- *c* is the concentration, *x* is the position on the river, *t* is the amount of time that passes, *D* is the diffusion factor, *u* is the velocity of the river, and *f* is the source or sink. The dimensions of the terms and coefficients in the equation are as follows-

$$c_t = \left[\frac{concentration}{T}\right], \ c_x = \left[\frac{concentration}{L}\right], \ c_{xx} = \left[\frac{concentration}{L}\right], \ c_{xx} = \left[\frac{concentration}{L^2}\right], \ D = \left[\frac{L^2}{T}\right], \ u = \left[\frac{L}{T}\right] \text{and } f = \left[\frac{concentration}{T}\right].$$

The derivation of equation (1) is as follows-

The time rate of change in concentration amount of contaminants due to a tributary in the interval from point a to point b in the river is represented by

$$A\int_{a}^{b}f_{0}(x,t)dx....(3)$$

where A is the cross-sectional area of the river and f0 is the source/sink. The total amount of contaminant in the river on the interval (a, b), is given by

$$A\int_{a}^{b}c(x,t)dx\dots\dots(4)$$

The flux in concentration across a plane due to diffusion is the amount of concentration that passes through this plane due to the diffusion process. According to Fick's Law of Diffusion, the concentration flux due to diffusion across any cross-section at a point *a* is proportional to the product of the cross-sectional area and the concentration gradient c_x . The flux in concentration due to diffusion at the points *a* and*b* with c_x being the concentration gradient is given by respectively.

and

$$-AD(b,c(b,t))c_x(b,t)\dots\dots(6)$$

 $-AD(a,c(a,t))c_{x}(a,t)\dots\dots(5)$

The concentration flux due to advection across any cross-section at point x is proportional to the product of the velocity, cross-sectional area, and concentration. By conservation of mass, we have

time rate of change = diffusion flux at (x=a) - diffusion flux at (x=b) + advection flux at(x=a) - advection flux at (x=b) + sources or sinks,

or equivalently,

$$\frac{d}{dt}A\int_{a}^{b}cdx = -AD(ac(a,t))c_{x}(a,t) + AD(b,c(b,t))c_{x}(b,t) + uAc(a,t) - uAc(b,t) + \int_{a}^{b}f_{0}(x,t)dx.....(7)$$

Now, divide through by A and let ($(f_0/A) = f$). Using the fundamental theorem of calculus,

$$\int_{a}^{b} \frac{d}{dx} f(x) dx = f(b) - f(a) \dots \dots \dots (8)$$

the result is

$$\int_{a}^{b} [(c)_{t} - (Dc_{x})_{x} + (uc)_{x} - f] dx = 0 \dots \dots \dots (9)$$

The choices of points *a* and *b* are arbitrary, so the integral equation is written as the partial differential equation

$$c_t - (Dc_x)_x + (uc)_x = f \dots \dots \dots (10)$$

Assume that there is no source or sinks holds (f = 0) and let *D* and *u* be constants. The final equation appears as

$$c_t + uc_x - Dc_{xx} = 0$$

Implies that

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2} \dots \dots \dots \dots (11)$$

2.2 ANALYTICAL SOLUTION

By coordinate transformation, the exact solution of the advection-diffusion equation in unbounded is given by [1]

$$C(x,t) = \frac{M}{A\sqrt{4\pi Dt}} exp\left(-\frac{(x-(x_0 + ut))^2}{4Dt}\right).....(12)$$

where, M = mass of the pollutant

A = cross sectional area perpendicular to x with the initial condition $c(x,0)=(M/A)\delta(x)$, where $\delta(x)$ is the Dirac delta function.

3. NUMERICAL METHOD FOR GOVERNING EQUATION

We consider the one-dimensional water pollution model problem as an initial and boundary value problem.

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} = D \frac{\partial^2 C}{\partial x^2} \dots \dots \dots \dots \dots (13)$$

With initial condition

$$c(t_0, x) = c_0(x); \qquad a \le x \le b$$

and boundary conditions

$$\begin{split} c(t,a) &= c_a(x); \qquad t_0 \leq t \leq T \\ c(t,b) &= c_b(x); \qquad t_0 \leq t \leq T \end{split}$$

Finite difference techniques for solving the one dimensional advection diffusion equation can be considered according to the number of spatial grid points involved, the number of time levels used, whether they are explicit or implicit nature.

In Mathematics, the finite difference methods (FDM) are numerical methods for solving differential equations by approximating them with difference equations, in which finite differences approximate the derivatives. FDMs are thus discretization methods.

Today, FDMs are the dominant approach to numerical solutions of partial differential equations. Our goal is to approximate solutions to differential equations. i.e. to find a function (or some discrete approximation to this functions) which satisfies a given relationship between various of its derivatives on some given region of space/and or time, along with some boundary conditions along the edges of this domain. In general, this is a difficult problem and rarely an analytic formula can be found for the solution. A finite difference method proceeds by replacing the derivatives in the differential equation by the finite difference approximations. This gives a large algebraic system of equation to be solved in place of the differential equation, something that is easily solved on a computer.

3.1 EXPLICIT CENTERED DIFFERENCE SCHEME BY FTBSCS TECHNIQUES

Consider the model equation $\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2} \dots \dots \dots (14)$ In order to develop the scheme, we discretize the *x*-*t* plane by choosing a mesh width $h \equiv \Delta x$ space size and a time step size $k \equiv \Delta t$. The finite difference methods, we will develop, produce approximations $c_i^n \in \mathbb{R}^n$ to the solution $c(x_i, t_n)$ in the discrete points by

> $x_i = ih, \quad i = 0, 1, 2, 3, \dots, \dots$ $t_n = nk, \quad n = 0, 1, 2, 3, \dots, \dots$

Let the solution $c(x_i, t_n)$ be denoted by C_i^n and its approximate value by c_i^n .

By Explicit upwind time difference formula $\frac{\partial C}{\partial t} = \frac{C_i^{n+1} - C_i^n}{\Delta t} \dots \dots \dots (15)$

Next use the backward space difference formula

And centered space difference formula

$$\frac{\partial^2 C}{\partial x^2} = \frac{C_{i+1}^n - 2C_i^n + C_{i-1}^n}{\Delta x^2} \dots \dots \dots (17)$$

Substituting equations (15 - 17) into equation (14) and rearrange according the time level, lead to

$$\frac{C_i^{n+1} - C_i^n}{\Delta t} + u \frac{C_i^n - C_{i-1}^n}{\Delta x} = D \frac{C_{i+1}^n - 2C_i^n + C_{i-1}^n}{\Delta x^2}$$

Which leads to

$$C_i^{n+1} = C_i^n - \frac{u\Delta t}{\Delta x} (C_i^n - C_{i-1}^n) + \frac{D\Delta t}{\Delta x^2} (C_{i+1}^n - 2C_i^n + C_{i-1}^n)$$

$$\therefore C_i^{n+1} = \left(\frac{u\Delta t}{\Delta x} + \frac{D\Delta t}{\Delta x^2}\right) C_{i-1}^n + \left(1 - \frac{u\Delta t}{\Delta x} - 2\frac{D\Delta t}{\Delta x^2}\right) C_i^n + \frac{D\Delta t}{\Delta x^2} C_{i+1}^n$$

Implies to

$$C_{i}^{n+1} = (\gamma + \lambda) * C_{i-1}^{n} + (1 - \gamma - 2 * \lambda) * C_{i}^{n} + \lambda * C_{i+1}^{n} \dots \dots \dots (18)$$

In which

$$\gamma = \frac{u\Delta t}{\Delta x}$$
, $\lambda = \frac{D\Delta t}{\Delta x^2}$

3.2 STABILITY CONDITIONS FOR THE SCHEME BY FTBSCS TECHNIQUES

The explicit centered difference scheme for (14) is given by

$$C_{i}^{n+1} = (\gamma + \lambda) * C_{i-1}^{n} + (1 - \gamma - 2 * \lambda) * C_{i}^{n} + \lambda * C_{i+1}^{n} \dots \dots \dots (19)$$

In which

$$\gamma = \frac{u\Delta t}{\Delta x}$$
, $\lambda = \frac{D\Delta t}{\Delta x^2}$

The equation (19) implies that if $0 < v + \lambda < 1$ (i)

$$0 \le \gamma + \lambda \le 1 \dots \dots \dots (I)$$

$$0 \le 1 - \gamma - 2\lambda \le 1 \dots \dots$$
 (ii)

 $0 \le \lambda \le 1 \dots \dots$ (iii)

then the new solution is a convex combination of the two previous solutions. That is, the solution at new time-step (n+1) at a spatial node *i* is an average of the solutions at the previous time-step at the spatial-nodes *i*-1, *i* and *i*+1. This means that the extreme value of the new solution is the average of the extreme values of the previous two solutions at the three consecutive nodes. Therefore, the new solution continuously depends on the initial value c_{i}^{0} , $i = 1, 2, 3, \dots, M$.

(ii) implies
$$\gamma \leq 1 - 2\lambda \leq 1 + \gamma \dots \dots$$
 (iv)

(i) implies
$$-\lambda \le \gamma \le 1 - \lambda$$

 $\therefore -\lambda \le \gamma \le 1 - 2\lambda$ by (iv)

Therefore,

the conditions are $0 \le \lambda \le 1$ and $-\lambda \le \gamma \le 1 - 2\lambda$ That is $0 \le \frac{D\Delta t}{\Delta x^2} \le 1$ and $-\frac{D\Delta t}{\Delta x^2} \le \frac{u\Delta t}{\Delta x} \le 1 - 2\frac{D\Delta t}{\Delta x^2}$ are the st ability conditions of (19).

4. ALGORITHM FOR THE NUMERICAL SOLUTION

To find the numerical solution of the model, we have to accumulate some variables which are offered in the following algorithm.

Input:*nx* and *nt*are the number of spatial and temporal mesh points respectively.

 t_{f} , the right end of (0, T)

 x_d , the right end point of (0, b)

 C_0 , the initial concentration density, apply as initial condition

C_a, left hand boundary condition

C_b, right hand boundary condition

D, diffusion rate

u, velocity

Output: C(x, t), the solution matrix Initialization: $dt = \frac{T-0}{nt}$, the temporal grid size

$$dx = \frac{b-0}{nx}$$
, the spatial grid size
 $gm = \frac{u*dt}{dx}$, the courant number
 $ld = \frac{D*dt}{(dx)^2}$ (peclet number)

Step 1. Calculation for concentration profile of explicit centered difference scheme forn=1 to *nt*

for *i*=2 to *nx* $C(n + 1, i) = (\gamma + \lambda) * C(n, i - 1) + (1 - \gamma - 2 * \lambda) * C(n, i)$ $+ \gamma * C(n, i + 1)$

end end

Step 2: output *C*(*x*, *t*) Step 3: Figure Presentation Step 4: Stop

5. COMPUTATIONAL RESULTS

5.1. ERROR ESTIMATION AND CONVERGENCE

We have discussed two types of explicit finite difference schemes in the previous sections.

Now, we compute the relative error of the explicit differ ence scheme by using FTBSCS technique which is defined by the relative error in L_1 – norm as

$$err = \frac{\parallel C_e^{\perp} - C_n \parallel_1}{\parallel C_n \parallel} \dots \dots \dots \dots \dots (20)$$

where, C_e is the exact solution and C_n is the numerical solution computed by the finite difference scheme by FTBSCS techniques for time $t \in [0, 6]$.

The following figure 5.1 shows the convergence of relative error by the scheme FTBSCS techniques.

Numerical computation of ADE is presented by using explicit finite difference methods by FTBSCS techniques and compared with an exact solution of the ADE. A good agreement between the numerical solutions and the analytical solutions are obtained and the error becomes clear when using large size step for time. The choice of smaller discretization parameters (δ tand δ x) produce less errors. However we can say that FTBSCS techniques show the stable and accurate solutions for the advection diffusion equation.

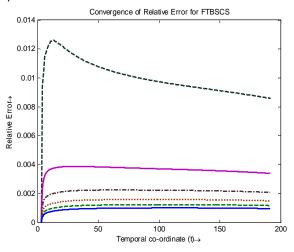


Figure 5.1 Rate of Numerical feature of Convergence.

5.2 NUMERICAL SIMULATION AND RESULTS DISCUSSIONS

This section presents the numerical simulation results for pollutant transportation in river water with increasing water flow velocity and increasing diffusion coefficient. To test the accuracy of the numerical scheme by FTBSCS technique for the ADE, we implement the model for some artificial data for the transport of the pollutant in the river water. Our aim is to show that for the water pollution, any substance with bigger diffusion results a wider pollutant front or a bigger diffusion distance. For different coefficients ranging from $9m^2/s$ to 25 m^2/s , as shown in figures 5.2 to 5.4.

Problem description: Estimation of pollutant in a river of length=600 m=0.6 km at all time t = 1min to t = 6 min.

If u = 1 m/s = 3.6 km/h and $D = 25 \text{ m}^2/\text{s}$ at time from 1 min to 6 min, for the numerical scheme FTBSCS technique is shown in Figure 5.2. Which shows that the pollutant distribution within the described domain.

1 min 0.9 2 min •••••• 3 min 0.8 5 min 07 '6 min Mass fraction(cn) 0.6 0.5 04 0.3 0.2 0.1 0 100 200 300 400 500 600 0 Spatial co-ordinate (x)→

Numerical solution of 1D ADE taking u=1 m/s, D=16 m/s

Figure 5.2:1D ADE with u = 1 m/s = 3.6 km/h and $D = 9 \text{ m}^2/\text{s}$.

The curve marked by "solid line" shows the concentration profile for 1 minute (left), the curve visible by "dash line" represents the concentration profile for 2 minutes(left). The curve "dot line" shows the concentration profile for 3 minutes, the curve visible by "dash-dot line" represents the concentration profile for 4 minutes, The "solid line" curve shows the concentration profile for 5 minutes (right) and the curve visible by "dash line" represents the concentration profile for 6 minutes(right). We have seen that the pollutant concentration is increasing with respect to time increasing.

Now, we observe the following different figures for different diffusion coefficients and for different velocities. If u = 1 m/s = 3.6 km/h and varying the diffusion rate a time t = 6 min, the solution appeared is given below:

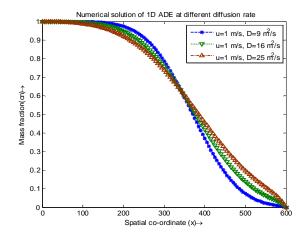


Figure 5.3:1D ADE with u=1 m/s=3.6 km/h and varying the diffusion rate at time 6 min.

If $D = 9 m^2/s$ and varying the velocity at time 6 min, the solution appeared is given below:

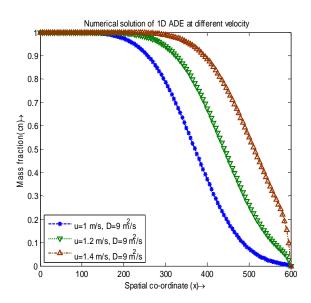


Figure 5.3:1D ADE with diffusion D = 9 m²/s = 3.6 km/h and varying the velocity at time 6 min.

If varying both velocity and diffusion coefficient at time 6 *min*, the solution appeared is given below:

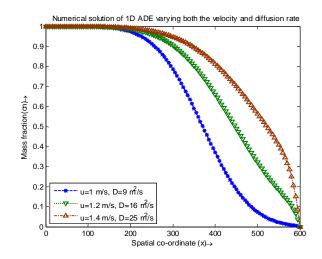


Figure 5.4:1D ADE with varying both the velocity and diffusion at time 6 min.

As we know the stability conditions of the scheme by FTBSCS technique are $0 \le \frac{D\Delta t}{\Delta x^2} \le 1$ and $-\frac{D\Delta t}{\Delta x^2} \le \frac{u\Delta t}{\Delta x} \le 1 - 2\frac{D\Delta t}{\Delta x^{2'}}$ this course of action will be continued until this stability conditions are satisfied. From this conditions, we have the diffusivity coefficient ranges from $D = 9 m^2/s$ to $25 m^2/s$ and the velocity ranges from 1 m/s to 1.4 m/s.

6. CONCLUSION

In this paper, analytical solutions and numerical solutions for 1D advection diffusion equation, with an initial condition and two boundary conditions, have been presented. The ADE has been considered as model equation for estimation of water pollution by using explicit finite difference scheme (FTBSCS techniques). We have computed relative errors for the scheme which shows a good rate of convergence of the numerical scheme. So, the scheme (FTBSCS techniques) for ADE is stable and consistent.

Also, we have presented the numerical solutions graphically by varying the value of velocity and value of diffusion coefficient. The graphical presentations are verifying the qualitative behavior of the solutions of ADE for various considerations of the parameters. The results show that the water pollutions are spreading with varying the diffusion term and advection term with respect to time and space.

This method can be extended for higher dimensional ADE as a water pollution model which demands the further study.

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